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# Hybrid Model Predictive Control of Chiller Plant with Thermal Energy Storage Evaluated with Modelica-Python Co-Simulation

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# Outline

- Background: Demand Response for Chiller Plant System
- Challenges and Proposed Work
- Chiller Plant with Water Storage: System Configuration & Modelica Dynamic Simulation Model
- Control-oriented Modeling: Koopman Models & Model Selection
- Hybrid Model Predictive Control for Demand Response Operation
- Simulation Study with Python-Modelica Co-Simulation Platform

#### Background





Source: ©2013 2030, Inc. / Architecture 2030. All Rights Reserved. Data Source: U.S. Energy Information Administration (2012).

U.S. primary energy consumption by energy source, 2021





Average Day (Time)

- Significant share of building energy consumption and electricity use
- Grid stability under increasing penetration of renewable energy

- Development of Gridinteractive Efficient Buildings
- Demand response and ancillary services by building HVAC operation

Data source: U.S. Energy Information Administration, *Monthly Energy Review*, Table 1.3 and 10.1, April 2022, preliminary data

Cia Note: Sum of components may not equal 100% because of independent rounding.

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## Review of Existing Work

Two key challenges:

- significant nonlinearities of plant characteristics are present;
- continuous and discontinuous manipulated variables coexist, due to the on/off and/or staged operation of some actuating devices in addition to the continuously adjustable devices.

Existing solution:

- Conventional scheduling techniques
- Operation shift with Thermal Energy Storage
- ➢ Piecewise linearization
- > Mixed-integer linear programming model predictive control (MILP-MPC) strategy

M. Fadzli Haniff, H. Selamat, R. Yusof, S. Buyamin, and F. Sham Ismail, "Review of hvac scheduling techniques for buildings towards energy-efficient and cost-effective operations," Renewable and Sustainable Energy Reviews, vol. 27, pp. 94–103, 2013.

M. J. Risbeck, C. T. Maravelias, J. B. Rawlings, and R. D. Turney, "A mixed-integer linear programming model for real-time cost optimization of building heating, ventilation, and air conditioning equipment," Energy and Buildings, vol. 142, pp. 220–235, 2017.



## **Proposed Work**

Motivations:

- Demand responds for energy saving
- Global optimization with mixed-integer nonlinear programming MPC

• Chiller plant with thermal energy storage (TES) system



- Data-driven control-oriented model with Koopman operators for different operation modes
  - Hybrid dynamical system with mode switch (mixed-integer bilinear term)
- Model predictive control on temperature regulation and minimization power consumption

• Convexification for mixed-integer bilinear term (facilitate computing)

Mixed-integer bilinear programming  $\rightarrow$  mixed-integer linear programming

## **Dynamic Simulation Plant**

• Modelica dynamic simulation plant: a chiller plant with thermal energy storage

#### Components

- Scroll compressor (4 L displacement)
- A counter flow wet cooling tower
- A shell and tube condenser
- A shell and tube evaporator
- A stratified tank for thermal energy storage
- Refrigerant: R134a

1: EEV opening → superheat
 2: compressor speed → leaving water
 temperature



Fig. 1. Schematic for Chiller Plant Coupled with Thermal Energy Storage

#### Dymola Layout for Chiller Plant and TES



Base on TLK library:

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T.-T. GmbH. TIL Suite. [Online]. Available: https://www.tlkthermo.com/index.php/en/til-suite



Base on Building library:

M. Wetter, W. Zuo, T. S. Nouidui, and X. Pang, "Modelica Buildings library," Journal of Building Performance Simulation, vol. 7, no. 4, pp. 253–270, 2014.

Dassault Systèmes, (2019), Dymola. Available: http://www.3ds.com/products/catia/portfolio/dymola.



## Illustration for Two Operation Modes





#### Mode 1: TES Charging

- TES charged by chiller water from chiller plant
- Building load (AHU) handled by chilled water from chiller plant
- Building/AHU return water + TES outlet water,  $\rightarrow$  chiller plant

#### Mode 2: TES Discharging

- TES discharges chiller water to AHU
- AHU supplied chill water comes from Chiller Plant and TES
- The AHU return water  $\rightarrow$  the TES and Chiller Plant

## Control-oriented Model for Chiller Plant with Water Storage

#### States:

- Chiller plant related states:
- $\succ$  compressor discharged pressure ( $P_{cd}$ )
- $\succ$  compressor discharge temperature ( $T_{cd}$ )
- $\succ$  compressor suction pressure ( $P_{cs}$ )
- Building load/AHU related state:
- > chilled-water return temperature  $(T_r)$
- Thermal energy storage related states:
- > top- and bottom-layer water temperatures ( $T_a$  and  $T_b$ )

#### Disturbance:

- > ambient temperature ( $T_{amb}$ )
- $\succ$  building load ( $\dot{Q}_{ld}$ ),

#### Inputs:

- $\succ$  tower fan speed ( $\dot{m}_{tf}$ )
- > chiller evaporator leaving water setpoint  $(T_{lwSP})$
- > chiller evaporator water mass flow rate  $(\dot{m}_{ew})$ ,

#### mode switch input: $\delta \in \{0, 1\}$ , where 0 represents Mode 1 and 1 represents Mode 2

#### Power consumption(*P*<sub>t</sub>):

- compressor power (P<sub>cmp</sub>)
- > tower fan power ( $P_{tf}$ )
- evaporator liquid pump power(Ppmp)

#### Data-driven model with Koopman operators for Mode 1&2

**Original States:** 

$$x = [P_{cd}, T_{cd}, P_{cs}, T_r, T_a, T_b]^T$$

Inputs:

$$u = [\dot{m}_{tf}, T_{lwSP}, \dot{m}_{ew}]^T$$

Disturbance:

 $w = [T_{amb}, \dot{Q}_{ld}]^T$ 

Discrete-time dynamic system:  $x_{k+1} = F(x_k, u_k, w_k)$ 



finite-dimensional lifted space  $z_{k+1} = Az_k + B_u u_k + B_w w_k$   $\hat{x}_k = Cz_k$   $\clubsuit$ Kernel function  $z \triangleq \boldsymbol{\psi}(x) = [\psi_1(x) \quad \cdots \quad \psi_N(x)]^T$ 

 In this study, the original states x are affined into the 1storder, 2nd-order polynomial functions and their cross terms.

$$z = [x_1, \ldots, x_6, x_1^2, \ldots, x_6^2, x_1x_2, \ldots, x_5x_6]^T$$

## Sparse Identification of Nonlinear Dynamics with Control (SINDYc)

$$z = [x_1, \dots, x_6, x_1^2, \dots, x_6^2, x_1x_2, \dots, x_5x_6]^T$$

$$\operatorname{argmin}_{A,B} \|\Xi_+ - A\Xi - B_u \mathbf{U} - B_w \mathbf{W}\|_2$$

$$\operatorname{Mode 1:} z_{k+1}^1 = A^1 z_k^1 + B_u^1 u_k^1 + B_w^1 w_k^1$$

$$\operatorname{Mode 2:} z_{k+1}^2 = A^2 z_k^2 + B_u^2 u_k^2 + B_w^2 w_k^2$$

$$\cdot \text{Typical Akaike Information Criterion (AIC) for polynomial functions} \qquad \operatorname{Alsize, H} (1969). \text{Fitting antergenetive models for prediction. Another back State. Model}, z_{101, 249-247}^{AIC}$$

$$\operatorname{Residual Sum of Squares for fitting error}_{AIC Score \longrightarrow AIC} = \rho \cdot \ln \left(\frac{RSS}{\rho} + 2p\right)^{-1} \text{Maximum likelihood function}}$$

$$\cdot \text{ AIC with correction (AICc) for small sample size: } AIC_c = AIC + \frac{2(p+1)(p+2)}{(p-\rho-2)}$$

$$\cdot \text{ The total power model for two modes is identified as a static map of all states, inputs and disturbances.}$$

$$\operatorname{Mode 2:} y_k^2 = C^2 z_k^2 + D_u^2 u_k^2 + D_w^2 w_k^2$$

#### Model Selection Results for Mode 1 (600s sampling time)



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#### Model Selection Results for Mode 2 (600s sampling time)



#### Hybrid system model by mixed dynamical system

$$z_{k+1} = \begin{cases} A^{1}z_{k} + B^{1}_{u}u_{k} + B^{1}_{w}w_{k}, & \delta_{k} = 0, \\ A^{2}z_{k} + B^{2}_{u}u_{k} + B^{2}_{w}w_{k}, & \delta_{k} = 1. \end{cases}$$
$$y_{k} = \begin{cases} C^{1}z_{k} + D^{1}_{u}u_{k} + D^{1}_{w}w_{k}, & \delta_{k} = 0, \\ D^{2}z_{k} + D^{2}_{u}u_{k} + D^{2}_{w}w_{k}, & \delta_{k} = 1. \end{cases}$$

Mixed-integer dynamic model with bilinear terms

$$z_{k+1} = (A^1 - A^2) z_k \delta_k + (B^1_u - B^2_u) u_k \delta_k + (B^1_w - B^2_w) w_k \delta_k + A^2 z_k + B^2_u u_k + B^2_w w_k$$

$$y_{k} = (C^{1} - C^{2})z_{k}\delta_{k} + (D_{u}^{1} - D_{u}^{2})u_{k}\delta_{k} + (D_{w}^{1} - D_{w}^{2})w_{k}\delta_{k} + C^{2}z_{k} + D_{u}^{2}u_{k} + D_{w}^{2}w_{k}$$

## HMPC for Chiller Plant with Water Storage

HMPC design problem: minimizing energy cost while regulating AHU return water temperature requirements, assuming perfect knowledge of future ambient temperature and cooling load



#### Convexification for bilinear programming

Define the new variables of bilinear functions

$$f_z(z,\delta) = z\delta$$
  $f_u(u,\delta) = u\delta$ 

Convex hulls

$$conv(\mathcal{S}_{z,i}) = \{ (z_i, \delta, f_{z,i}) \in (\mathbb{R} \times \mathbb{I} \times \mathbb{R}) | \mathcal{F}_{z,i} \}$$
$$conv(\mathcal{S}_{u,j}) = \{ (u_j, \delta, f_{u,j}) \in (\mathbb{R} \times \mathbb{I} \times \mathbb{R}) | \mathcal{F}_{u,j} \}$$

$$\mathcal{F}_{z} = \begin{cases} f_{z} \geq z^{lb}\delta + \delta^{lb}z - z^{lb}\delta^{lb} \\ f_{z} \geq z^{ub}\delta + \delta^{ub}z - z^{ub}\delta^{ub} \\ f_{z} \leq z^{lb}\delta + \delta^{ub}z - z^{lb}\delta^{ub} \\ f_{z} \leq z^{ub}\delta + \delta^{lb}z - z^{ub}\delta^{lb} \end{cases}$$
$$\mathcal{F}_{u} = \begin{cases} f_{u} \geq u^{lb}\delta + \delta^{lb}u - u^{lb}\delta^{lb} \\ f_{u} \geq u^{ub}\delta + \delta^{ub}u - u^{ub}\delta^{ub} \\ f_{u} \leq u^{lb}\delta + \delta^{ub}u - u^{lb}\delta^{ub} \\ f_{u} \leq u^{ub}\delta + \delta^{lb}u - u^{lb}\delta^{ub} \\ f_{u} \leq u^{ub}\delta + \delta^{lb}u - u^{ub}\delta^{lb} \end{cases}$$

MILP-MPC

$$\min_{\substack{u,\delta,f_z,f_u}} \left[ \sum_{k=0}^{N_p-1} (q_{\delta}^T f_{z,k} + r_{\delta}^T f_{u,k} + p_{\delta}^T w_k \delta_k + q_z^T z_k + r^T u_k + p_{\delta}^T w_k + q_z^T z_k + r^T u_k + p_{\delta}^T w_k + q_z^T z_k + r^T u_k + p_{\delta}^T w_k + q_z^T z_k + r^T u_k + q_z^T z_k + r^T u_k$$

*s.t*.

$$z_{k+1} = A^3 f_{z,k} + B^3_u f_{u,k} + B^3_w w_k \delta_k$$
  
+  $A^2 z_k + B^2_u u_k + B^2_w w_k$   
 $z^{lb}_k \leq z_k \leq z^{ub}_k, u^{lb}_k \leq u_k \leq u^{ub}_k$   
 $z_0 = z_{ini}$   
 $k \in \mathbb{I}_{[0,N_p)}$ 

# Hybrid Model Predictive Control with mixed-integer bilinear programming (HMPC-MIBLP)

- Dymola: Modelica model of Chiller Plant with Water Storage
- Python: MPC design and implementation

FMI 2.0 Co-simulation



https://fmi-standard.org/

#### **Simulation setting**

- Sampling time : 600s
- Predictive horizon : 2 hours
- Initial tower fan speed: 40 Hz
- Initial chiller leaving water temperature setpoint: 10 °C
- Initial chiller plant water mass flow rate: 11 kg/s
- Initial TES charging/discharging mode: 1 (discharging)
- Initial ambient temperature: 28 °C
- Initial cooling load on AHU cooling coil: 360 kW

#### Utilized Python package:

Created on Sat Sep 17 14:54:36 2022
@author: cxp161130 """
import cvxpy as cp
import numpy as np
import scipy as sp
from scipy import sparse
<pre>import matplotlib.pyplot as plt</pre>
<pre># from matplotlib.patches import StepPatch</pre>
import shutil
import scipy.io as scio
import time
<pre>from fmpy import read_model_description, extract</pre>
from fmpy.fmi2 import FMU2Slave

Diamond, S., & Boyd, S. (2016). CVXPY: A Python-embedded modeling language for covex optimization. *J. Machine Learning Res.*, 17(83), 1–5. https://doi.org/10.48550/arXiv.1603.00943.

T. Sommer, FMPy, (2020). Available online: https://github.com/CATIA-Systems/FMPy.



low-price region (LPR: [0, 14.5] hour) medium-price region (MPR: [14.5, 17.5] hour) high-price region (HPR: [17.5, 24] hour)



Oscillation due to mode switch and inner PI controllers





## Conclusion

- We propose a data-driven method of Chiller plant coupled with chilled-water storage.
- The SINDYc-based Koopman-invariant subspace models are identified with simulations data from Modelica-based dynamics model.
- A MIBLP-MPC is formulated for global optimization of energy saving and satisfication of cooling rate demand.
- To solve this optimization problem, a convexification with McCormick envelopes is implemented and transformed the MIBLP into MILP.
- The proposed control strategy is evaluated with Python-based cosimulation framework.

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# Thanks!

# Any Questions?